

Code No: 156BC

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JAWAHARLAL NEHRU TECHNOLOGICAL UNIVERSITY HYDERABAD

B. Tech III Year II Semester Examinations, February/March - 2022

HEAT TRANSFER
(Mechanical Engineering)

Time: 3 hours

Max. Marks: 75

Answer any five questions
All questions carry equal marks

- 1.a) Derive steady state general Heat conduction equation without heat generation in cylindrical systems.
- b) Write down the equation for conduction of heat through a slab or Plane wall. [10+5]
- 2.a) List the assumptions made while analyzing the heat flow from a finned surface.
- b) A 2cm thick steel slab heated to 525°C is held in air stream having a mean temperature of 25°C . Estimate the time interval when the slab temperature would not depart from the mean value of 25°C by more than 0.5°C at any point in the slab. The steel plate has the following thermos-physical properties: $\rho = 7950 \text{ kg/m}^3$, $c_p = 455 \text{ J/kg}^{\circ}\text{C}$, $k = 46 \text{ W/m}^{\circ}\text{C}$.h (heat transfer coefficient on plate surface) = $36 \text{ W/m}^2^{\circ}\text{C}$. [5+10]
- 3.a) What are repeating variables and how are they selected for dimensional analysis?
- b) 3000 kg of water is heated per hour from 30°C to 70°C by pumping it through a certain heated section of a 25 mm diameter tube. If the surface of the heated section is maintained at 110°C , estimate length of the heated section and the rate of heat transfer from the tube to water. [5+10]
- 4.a) Derive an expression for LMTD for a Parallel Flow Heat Exchangers.
- b) A hot square plate of $75 \text{ cm} \times 75 \text{ cm}$ at 120°C is exposed to atmospheric air at 40°C . Find the heat lost from both surfaces of the plate if it is kept in vertical position. [8+7]
- 5.a) Water is boiled at atmospheric pressure by a horizontal polished copper heating element of diameter $D = 5 \text{ mm}$ and emissivity $\epsilon = 0.05$ immersed in water. If the surface temperature of the heating wire is 350°C , determine the rate of heat transfer from the wire to the water per unit length of the wire.
- b) State and explain the Stefan-Boltzmann law of radiation heat transfer, giving the nomenclature involved in it. [8+7]
- 6.a) It is required to heat the oil to 300°C for frying purpose. A long ladle is used in frying pan. The section of the ladle is $5 \text{ mm} \times 18 \text{ mm}$. The surrounding air is at 30°C and the thermal conductivity of the ladle material is 205 W/mK . If the temperature at a distance of 380 mm from the oil should not exceed 40°C , determine convective heat transfer coefficient.
- b) Derive an expression for temperature distribution under steady state in one dimensional heat conduction for a plane wall. [8+7]

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7. An electrically heated thin foil of length $L = 25\text{mm}$ and width $W = 8\text{ mm}$ is to be used as a wind speed meter. Wind with a temperature T_∞ and velocity U_∞ blows parallel to the longest side. The foil is internally heated by an electric heater dissipating Q (Watts) from both sides and is to be operated in air with $T_\infty = 20^\circ\text{C}$, $C_p = 1.005\text{kJ/kg K}$, $\nu = 1.522 \times 10^{-5}\text{ m}^2/\text{s}$, $\rho = 1.19\text{ kg/m}^3$ and $Pr = 0.72$. The surface temperature, T_s of the foil is to be measured at the trailing edge - but can be assumed to be constant. Estimate the wind speed when $T_s = 32^\circ\text{C}$ and $Q = 0.5\text{ W}$. [15]

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8.a) How heat exchangers of classified.

b) A double-pipe (shell-and-tube) heat exchanger is constructed of a stainless steel ($k = 15.1\text{ W/m}^\circ\text{C}$) inner tube of inner diameter $D = 1.5\text{ cm}$ and outer diameter $D_o = 1.9\text{ cm}$ and an outer shell of inner diameter 3.2 cm . The convection heat transfer coefficient is given to be $h_i = 800\text{ W/m}^2^\circ\text{C}$ on the inner surface of the tube and $h_o = 1200\text{ W/m}^2^\circ\text{C}$ on the outer surface. For a fouling factor of $R_{f,i} = 0.0004\text{ m}^2^\circ\text{C/W}$ on the tube side and $R_{f,o} = 0.0001\text{ m}^2^\circ\text{C/W}$ on the shell side, determine:

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- i) The thermal resistance of the heat exchanger per unit length.
- ii) The overall heat transfer coefficients, U_i and U_o based on the inner and outer surface areas of the tube, respectively. [5+10]

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